

Homework Assignment Number Five
Assigned: Wednesday, February 10, 1999

Due: Wednesday, February 17, 1999 BEFORE LECTURE STARTS.

Problem 1. Geankoplis, problem 2.10-3, page 111

$$\rho = 801 \frac{\text{kg}}{\text{m}^3}, \mu = 1.49 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}}, \bar{v} = 4.57 \frac{\text{m}}{\text{s}}$$

$$D = 1.5'' @ \text{ schd } 40 = 0.04089\text{m}, L = 61\text{m}$$

$$N_{\text{Re}} = \frac{D\bar{v}\rho}{\mu} = 100467 \text{ therefore flow is turbulent}$$

$$(a) \quad \frac{\epsilon}{D} = \frac{4.6 \cdot 10^{-5}}{0.04089} = 0.00112$$

from table on page 88 of Geankoplis $f = 0.006$

$$F_f = \frac{4fL\bar{v}^2}{D^2} = 373.9 \frac{\text{J}}{\text{kg}}$$

(b)

from table on page 88 of Geankoplis $f = 0.004$

$$F_f = \frac{4fL\bar{v}^2}{D^2} = 249.3 \frac{\text{J}}{\text{kg}}$$

percent reduction:

$$\frac{373.9 - 249.3}{373.9} = 0.333$$

Problem 2. Geankoplis, problem 2.10-5, page 112

$$q = 0.223 \frac{\text{ft}^3}{\text{s}} \rho = 60.52 \frac{\text{lb}_m}{\text{ft}^3}, \mu = 2.33 \cdot 10^{-4} \frac{\text{lb}_m}{\text{ft} \cdot \text{s}},$$

$$D_{1.5} = 1.5'' @ \text{ schd } 40 = 0.1342\text{ft}, A_{1.5} = 0.01414\text{ft}^2$$

$$D_{2.5} = 2.5'' @ \text{ schd } 40 = 0.2058\text{ft}, A_{2.5} = 0.03322\text{ft}^2$$

$$\bar{v}_{1.5} = \frac{q}{A_{1.5}} = 15.77 \frac{\text{ft}}{\text{s}} \text{ and } \bar{v}_{2.5} = \frac{q}{A_{2.5}} = 6.71 \frac{\text{ft}}{\text{s}}$$

$$N_{\text{Re},1.5} = \frac{D_{1.5} \bar{v}_{1.5} \rho}{\mu} = 549702 \text{ therefore flow is turbulent in 1.5 inch pipe}$$

$$N_{\text{Re},2.5} = \frac{D_{2.5} \bar{v}_{2.5} \rho}{\mu} = 358683 \text{ therefore flow is turbulent in 2.5 inch pipe}$$

$$\frac{\epsilon}{D_{1.5}} = \frac{0.00015}{0.1342} = 0.00112 \text{ and } \frac{\epsilon}{D_{2.5}} = \frac{0.00015}{0.2058} = 0.00073$$

$$\text{from table on page 88 of Geankoplis } f_{1.5} = 0.0048, f_{2.5} = 0.0045$$

$$L_{1.5} = 20\text{ft}, L_{2.5} = 125 + 10 + 50 = 185\text{ft}$$

(a) Contraction loss at tank:

$$K_c = 0.55 \left(1 - \frac{A_{1.5}}{A_1} \right) = 0.55, h_{f,c} = K_c \frac{\bar{v}_{1.5}^2}{2g_c} = 2.12 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

(b) skin friction in 1.5 inch pipe:

$$F_{f,1.5} = \frac{4f_{1.5}L_{1.5}\bar{v}_{1.5}^2}{D_{1.5}2} = 11.05 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

(c) friction in 1.5 inch elbow:

$$h_{f,L,1.5} = K_L \frac{\bar{v}_{1.5}^2}{2g_c} = (0.75) \frac{\bar{v}_{1.5}^2}{2g_c} = 2.90 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

(d) Expansion loss in pipe:

$$K_x = \left(1 - \frac{A_{1.5}}{A_{2.5}} \right)^2 = 0.33, h_{f,x} = K_x \frac{\bar{v}_{1.5}^2}{2g_c} = 1.27 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

(e) skin friction in 2.5 inch pipe:

$$F_{f,2.5} = \frac{4f_{2.5}L_{2.5}\bar{v}_{2.5}^2}{D_{2.5}2} = 11.31 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

(f) friction in two 1.5 inch elbows:

$$h_{f,L,2.5} = K_L \frac{\bar{v}_{2.5}^2}{2g_c} = (0.75) \frac{\bar{v}_{2.5}^2}{2g_c} = 0.52 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

$$2h_{f,L,2.5} = 1.05 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

$$\sum F = h_{f,c} + F_{f,1.5} + h_{f,L,1.5} + h_{f,x} + F_{f,2.5} + 2h_{f,L,2.5} = 29.7 \frac{\text{ft} \cdot \text{lb}_f}{\text{lb}_m}$$

$$0 = \frac{\Delta p}{\rho} + \frac{1}{g_c} \frac{\Delta v^2}{2\alpha} + \frac{g}{g_c} \Delta z + \hat{W}_s + \sum \hat{F}$$

$$0 = 0 + \frac{6.71^2}{2} \frac{1}{32.2} + \Delta z + 0 + 29.7$$

$$\Delta z = -30.4 \text{ft}$$

Problem 3. Geankoplis, problem 2.10-8, page 112

$$(a) \quad \rho = \frac{\text{PMW}}{RT} = \frac{101325 \cdot 0.0288}{8.314 \cdot 283} = 1.24 \frac{\text{kg}}{\text{m}^3}$$

$$\mu = 0.0225 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}}, \quad \bar{v} = 2 \frac{\text{m}}{\text{s}}$$

$$D = 0.012 \text{m}$$

$$N_{\text{Re}} = \frac{D\bar{v}\rho}{\mu} = 1323 \quad \text{therefore flow is laminar}$$

$$L_e = 0.0575DN_{\text{Re}} = 0.91 \text{m}$$

$$(b) \quad \rho = 1000 \frac{\text{kg}}{\text{m}^3}$$

$$\mu = 1.307 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}}, \quad \bar{v} = 2 \frac{\text{m}}{\text{s}}$$

$$D = 0.012 \text{m}$$

$$N_{\text{Re}} = \frac{D\bar{v}\rho}{\mu} = 18363 \quad \text{therefore flow is turbulent}$$

$$L_e = 50D = 0.6 \text{m}$$

Problem 4. Geankoplis, problem 2.10-9, page 112

$$q = 3.494 \cdot 10^{-3} \frac{\text{m}^3}{\text{s}} \quad \rho = 833 \frac{\text{kg}}{\text{m}^3}, \quad \mu = 3.3 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}},$$

$$p_1 = 101325 + 345000 = 446325 \text{ Pa}$$

$$D_1 = 0.07792 \text{ m}, A_1 = 0.00477 \text{ m}^2$$

$$\bar{v}_1 = \frac{q}{A_1} = 0.7325 \frac{\text{m}}{\text{s}}$$

$$\dot{m} = \rho \bar{v}_1 A_1 = 2.91 \frac{\text{kg}}{\text{s}}$$

$$N_{\text{Re},1} = \frac{D_1 \bar{v}_1 \rho}{\mu} = 14407 \quad \text{therefore flow is turbulent}$$

$$\frac{\varepsilon}{D_1} = \frac{4.6 \cdot 10^{-5}}{0.07792} = 0.0006$$

from table on page 88 of Geankoplis $f_1 = 0.007$

$$L_1 = 120 \text{ m}$$

(a) Contraction loss at tank:

$$K_c = 0.55 \left(1 - \frac{A_{1.5}}{A_1} \right) = 0.55, h_{f,c} = K_c \frac{\bar{v}_{1.5}^2}{2} = 0.148 \frac{\text{J}}{\text{kg}}$$

(b) skin friction in pipe:

$$F_{f,1.5} = \frac{4f_1 L_1 \bar{v}_1^2}{D_1 2} = 11.78 \frac{\text{J}}{\text{kg}}$$

(c) friction in elbows:

$$h_{f,L,1} = K_L \frac{\bar{v}_1^2}{2} = (0.75) \frac{\bar{v}_1^2}{2} = 0.201 \frac{\text{J}}{\text{kg}}$$

$$2h_{f,L,1} = 0.403 \frac{\text{J}}{\text{kg}}$$

(d) valve

$$h_{f,v} = K_v \frac{\bar{v}_1^2}{2} = (9.5) \frac{\bar{v}_1^2}{2} = 2.55 \frac{\text{J}}{\text{kg}}$$

(e) Expansion loss:

$$K_x = \left(1 - \frac{A_1}{A_{\text{tank}}} \right)^2 = 1, h_{f,x} = K_x \frac{\bar{v}_1^2}{2} = 0.27 \frac{\text{J}}{\text{kg}}$$

$$\sum F = h_{f,c} + F_{f,1} + 2h_{f,L,1} + h_{f,v} + h_{f,x} = 15.15 \frac{\text{J}}{\text{kg}}$$

$$0 = \frac{\Delta p}{\rho} + \frac{1}{g_c} \frac{\Delta v^2}{2\alpha} + \frac{g}{g_c} \Delta z + \hat{W}_s + \sum \hat{F}$$

$$0 = \frac{\Delta p}{\rho} + \frac{\Delta v^2}{2\alpha} + g\Delta z + \hat{W}_s + \sum \hat{F}$$

$$0 = \frac{446325 - 101325}{833} + \frac{0.7325^2}{2} + 9.8(-20) + \hat{W}_s + 15.15$$

$$\hat{W}_s = -218.2 \frac{\text{J}}{\text{kg}}$$

$$\dot{W}_s = \hat{W}_s \dot{m} = -218.2 \cdot 2.91 = -635.0 \frac{\text{J}}{\text{s}}$$

$$\dot{W}_p = -\frac{\dot{W}_s}{\eta} = \frac{635}{0.65} = 977 \text{ W} = 1.0 \text{ kW}$$

Problem 5. Geankoplis, problem 2.10-10, page 112

$$q = 2.90 \cdot 10^{-3} \frac{\text{m}^3}{\text{s}}, L = 30 \text{ m}$$

$$D_1 = 1.0'' @ \text{ schd } 40 = 0.02664 \text{ m}, A_1 = 0.000557 \text{ m}^2$$

$$D_2 = 2.0'' @ \text{ schd } 40 = 0.05250 \text{ m}, A_2 = 0.002165 \text{ m}^2$$

$$\text{cross-sectional area: } A = A_2 - A_1 = 0.001608 \text{ m}^2$$

$$\text{wetted perimeter} = wp = \pi D_1 + \pi D_2 = 0.24863 \text{ m}$$

$$\bar{v} = \frac{q}{A} = 1.804 \frac{\text{m}}{\text{s}}$$

$$\text{density of water at } T = 45 \text{ C from appendix } \rho = 990.16 \frac{\text{kg}}{\text{m}^3}$$

$$\text{viscosity of water at } T = 45 \text{ C from appendix } \mu_a = 0.599 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}}$$

$$\text{viscosity of water at } T = 49 \text{ C from appendix } \mu_w = 0.559 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}}$$

$$d = 4r_H = 4 \frac{\text{cross-sectional-area}}{\text{wetted-perimeter}} = 0.02587 \text{ m}$$

$$N_{Re} = \frac{D\bar{v}\rho}{\mu} = 7.71 \cdot 10^4 \text{ therefore flow is turbulent}$$

$$\frac{\varepsilon}{D_1} = \frac{4.6 \cdot 10^{-5}}{0.02587} = 1.77 \cdot 10^{-3}$$

$$\text{from page 88 } f = 0.0057$$

$$\psi = \left(\frac{0.599 \cdot 10^{-3}}{0.559 \cdot 10^{-3}} \right)^{0.17} = 1.0118$$

$$F_f = \frac{4fL\bar{v}^2}{\psi D^2} = 42.52 \frac{\text{J}}{\text{kg}}$$

$$0 = \frac{\Delta p}{\rho} + \frac{1}{g_c} \frac{\Delta v^2}{2\alpha} + \frac{g}{g_c} \Delta z + \hat{W}_s + \sum \hat{F}$$

$$0 = \frac{\Delta p}{\rho} + 0 + 0 + 0 + 42.52$$

$$\Delta p = 42103 \text{ Pa}$$

Problem 6. Frymier, Assignment 5, problem 4 (SP.6) located at http://flory.engr.utk.edu/~frymier/che240/hw_list.html

$$q = 810 \frac{\text{gal}}{\text{min}} = 0.0511 \frac{\text{m}^3}{\text{s}} \quad \rho = 1180 \frac{\text{kg}}{\text{m}^3}, \quad \mu = 1.2 \cdot 10^{-3} \frac{\text{kg}}{\text{m} \cdot \text{s}},$$

$$D_1 = 6.0'' @ \text{schd } 40 = 0.1541 \text{ m}, \quad A_1 = 0.01865 \text{ m}^2$$

$$\bar{v}_1 = \frac{q}{A_1} = 2.740 \frac{\text{m}}{\text{s}}$$

$$\dot{m} = \rho \bar{v}_1 A_1 = 60.30 \frac{\text{kg}}{\text{s}}$$

$$N_{Re,1} = \frac{D_1 \bar{v}_1 \rho}{\mu} = 415189 \text{ therefore flow is turbulent}$$

$$\frac{\varepsilon}{D_1} = \frac{4.6 \cdot 10^{-5}}{0.1541} = 0.0003$$

$$\text{from table on page 88 of Geankoplis } f_1 = 0.0035$$

$$L_1 = 700 \text{ ft} = 213.36 \text{ m}$$

(a) Contraction loss at tank:

$$K_c = 0.55 \left(1 - \frac{A_1}{A_{\text{tank}}} \right) = 0.55, h_{f,c} = K_c \frac{\bar{v}_1^2}{2} = 2.06 \frac{\text{J}}{\text{kg}}$$

(b) skin friction in pipe:

$$F_{f,1.5} = \frac{4f_1 L_1 \bar{v}_1^2}{D_1 2} = 72.76 \frac{\text{J}}{\text{kg}}$$

(c) friction in elbows:

$$h_{f,L,1} = K_L \frac{\bar{v}_1^2}{2} = (0.75) \frac{\bar{v}_1^2}{2} = 2.82 \frac{\text{J}}{\text{kg}}$$

$$4h_{f,L,1} = 11.26 \frac{\text{J}}{\text{kg}}$$

(d) valves

$$h_{f,v} = K_v \frac{\bar{v}_1^2}{2} = (0.17) \frac{\bar{v}_1^2}{2} = 0.64 \frac{\text{J}}{\text{kg}}$$

$$2h_{f,v} = 1.28 \frac{\text{J}}{\text{kg}}$$

(d) tees

$$h_{f,T} = K_T \frac{\bar{v}_1^2}{2} = (1.0) \frac{\bar{v}_1^2}{2} = 3.75 \frac{\text{J}}{\text{kg}}$$

$$4h_{f,T,1} = 15.02 \frac{\text{J}}{\text{kg}}$$

(f) Expansion loss:

$$K_x = \left(1 - \frac{A_1}{A_{\text{tank}}} \right)^2 = 1, h_{f,x} = K_x \frac{\bar{v}_1^2}{2} = 3.75 \frac{\text{J}}{\text{kg}}$$

$$\sum F = h_{f,c} + F_{f,1} + 4h_{f,L,1} + 2h_{f,v} + 4h_{f,T,1} + h_{f,x} = 106.13 \frac{\text{J}}{\text{kg}}$$

$$0 = \frac{\Delta p}{\rho} + \frac{1}{g_c} \frac{\Delta v^2}{2\alpha} + \frac{g}{g_c} \Delta z + \hat{W}_s + \sum \hat{F}$$

$$\Delta p = \rho g H = 1180 \cdot 9.8 \cdot (200 \cdot 0.3048) = 704941 \text{ Pa}$$

$$0 = \frac{704941 \text{ Pa}}{1180} + 0 + 0 + \hat{W}_s + 106.13$$

$$\hat{W}_s = -703.5 \frac{\text{J}}{\text{kg}}$$

$$\dot{W}_s = \hat{W}_s \dot{m} = -703.5 \cdot 60.30 = -42423 \frac{\text{J}}{\text{s}}$$

$$\dot{W}_p = -\frac{\dot{W}_s}{\eta} = \frac{42423}{0.6} = 70705 \text{ W} = 94.8 \text{ hp}$$

(b)

$$\text{cost rate} = -\frac{0.56\$}{\text{kW} \cdot \text{hr}}$$

time = 24 hours

cost = rate*power*time

$$\text{cost} = 0.056 \cdot 70.705 \text{ kW} \cdot 24 \text{ hr} = \$95.03$$